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### Bubble Column Void Fraction and Bubble Size Measurement

Alexandra E. Sigel<sup>1,2</sup>, Manjil Ray<sup>1,2</sup>, Rodney O. Fox<sup>1,3</sup>, Alberto Passalacqua<sup>1,2,3</sup>, and Theodore J. Heindel<sup>1,2,3</sup> <sup>1</sup>Center for Multiphase Flow Research and Education <sup>2</sup>Department of Mechanical Engineering <sup>3</sup>Department of Chemical and Biological Engineering Iowa State University, Ames, IA, 50011, USA















## **Overview**

- Motivation
- Experimental setup and details
- Overall void fraction results
- Bubble size measurements
- Future work
- Conclusions













## **Motivation**

- Bubble column bioreactors are often used because of their desirable characteristics
- Scaleup of these bioreactors continues to be a challenge faced in chemical and fermentation industries
- Part of a larger project to validate computational fluid dynamic (CFD) tools to better understand the relationships between bubble column hydrodynamics and fermentation yield













# **Experimental Setup**

- 11 pressure transducers used to simultaneously measure pressure at various locations
- Gas is sparged through 8-arm spider sparger
- Column inner diameter of 32.1cm
- Fluid (water) static height is 10 column diameters or 3.21 meters











drain 4



# **Sparger Details**

- 8-arm spider sparger
- 26 1-mm holes in each arm arranged in 2 rows of 13 holes, with a 30° offset between rows
- Holes facing downward offset ±15° of bottom dead center
- Total open area ratio: 0.20%
- Height from bubble column base (h) is set at h = 31 mm but is adjustable (31 < h < 254 mm)





Sparger Section View





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# **Overall Void Fraction**

 Void fraction (also called volumetric gas fraction or gas holdup) determined by:

$$\varepsilon = 1 - \frac{\Delta P}{\Delta P_0}$$

- ε = void fraction between any two pressure transducers
- ∆P = average pressure drop between two pressure transducers when there is gas flow
- ∆P<sub>0</sub> = average pressure drop between two pressure transducers without gas flow

**Overall Void Fraction Comparison** 





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### **Bubble Column Void Fraction Data**



Superficial Gas Velocity

Source: Su, X., and Heindel, T.J., "Modeling Gas Holdup in Gas-Liquid-Fiber Semibatch Bubble Columns," *Industrial and Engineering Chemistry Research*, 44(24) 9355-9363 (2005).

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Source:

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# **Overall Void Fraction (cont.)**

**Overall Void Fraction Comparison** 

- Operating in pure heterogeneous regime due to sparger geometry and bubble coalescence
- Hysteresis is observed with "fresh" water but not after the column is operated for several hours
  - "fresh" water for trials 1 and 3





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# **Bubble Size Image Acquisition**

- 30.5 cm borescope inserted into the bubble column with exterior light sources paired with high-speed camera used for image collection
  - Others have used borescopes in homogeneous flows
- Images collected at multiple axial and radial locations paired with pre-selected superficial gas velocities
  - Superficial gas velocities for collection were determined from results and industry collaborator preferences













### **Borescope Image Analysis Challenges**



**Original Video** 

**Original Still Frame** 

**Binarized Frame** 

**Processed Frame** 

Verified Frame

- Image information:  $U_g = 2 \text{ cm/s}$ , 60 fps
- In-house image analysis code to determine bubble sizes by detecting bubble edges
- Bubbles that are isolated are easily identified. If there are bubbles 'stacked' the code cannot currently identify the edges effectively
  - Solved with lighting to create a broader range of intensities with the images
  - Currently improving process

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# **Next Steps**

- Improve image acquisition for bubble size distribution measures
- Use our X-ray flow visualization facility to complete X-ray Computed Tomography (XCT) imaging
  - Provides time-average local void fraction within the imaging region
- Introduce a fermentation broth simulant as the working fluid to conduct overall and local void fraction and bubble size measurements



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## Conclusions

- Bubble column bioreactors are used in the fermentation industry but are a challenge for scale-up
- Overall void fraction data provides information across a wide range of superficial gas velocities
- Operating in the pure heterogeneous regime provides challenges for bubble size distribution data collection
- Bubbles are captured with a borescope
  - Addressing imaging challenges











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